

# Development of Highly Efficient Raney Nickel Electrodes for Alkaline Water Electrolysis

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# Outline

- Introduction
- Electrode development by applying plasma spray technology
- Electrochemical results
- Cost reduction by applying atmospheric plasma spraying (APS)
- Electrode fabrication for power-to-gas plant in Wyhlen, Germany
- Summary



# HYSOLAR – Hydrogen from Solar Energy (1986-1995)

German - Saudi-Arabian project for solar hydrogen production

Erection of research and demonstration plants:

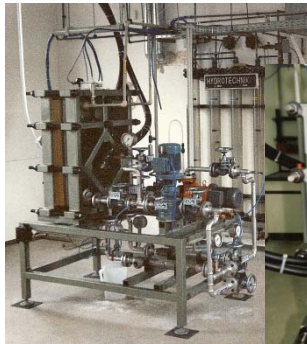
- Hydrogen production (350 kW in Riad, 10 kW in Stuttgart)
- Hydrogen usage (Hydrogen combustion engines, AFC, PAFC, catalytic burner)
- Total efficiency: 5,2 %,  
Efficiency PV panel: 8,1 %,  
Efficiency electrolyzer: 80,0 %



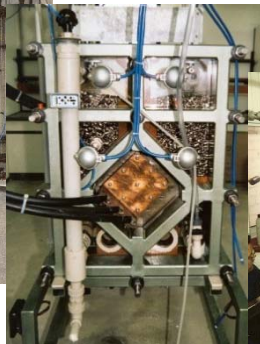


# Electrolyzers of HYSOLAR Project: Experimental/Test systems

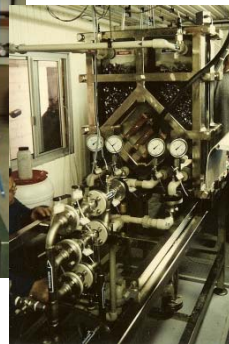
$P = 2 - 350/500\text{kW}$ ,  $p = 1 - 10\text{bar}_{\text{abs}}$ ,  $T = 40 - 95^\circ\text{C}$



HT



HT/DLR



HT/  
DLR



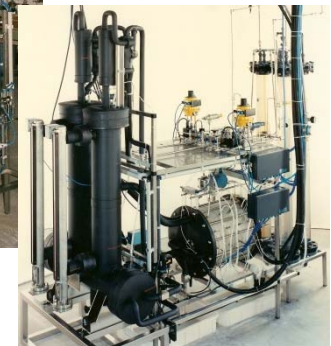
HS



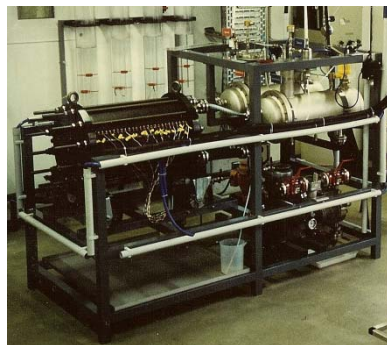
HS/DLR



MA



MA/DLR



FZJ



FZJ/DLR



FZJ/DLR

Supplier:

HYDROGEN SYSTEMS /  
METKON ALYZER 10kW

Supplier:

HYDROTECHNIK

3 / 2 kW

Supplier:

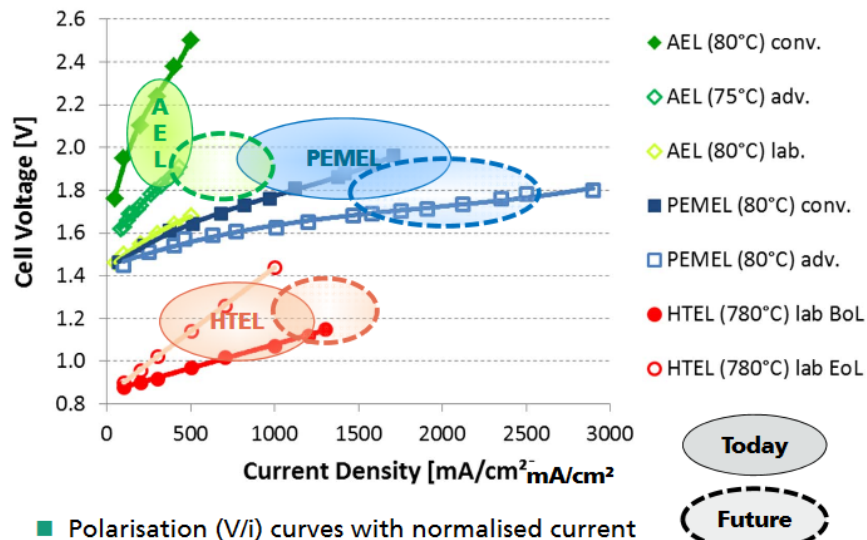
FZ JÜLICH

10 kW



# Targets of DLR Electrode Development

## (1) Performance and Efficiency of Water Electrolysis Comparison of different EL technologies at stack level.



Source:

<http://www.fch.europa.eu/sites/default/files/2%20Water%20Electrolysis%20Status%20and%20Potential%20for%20Development.pdf>

Performance: Operation at  $>0.6 \text{ A cm}^{-2}$  with a cell voltage of 1.8 V

Durability: 10 000 hours with 2 000 on-off cycles with less than 10% degradation

Cost: Reduction by 30% at stack level



# Benchmarked Catalyst for Alkaline Water Electrolysis

Raney Ni

100 mV overpotential at  $500 \text{ mA cm}^{-2}$

28 wt% KOH,  $80^\circ\text{C}$

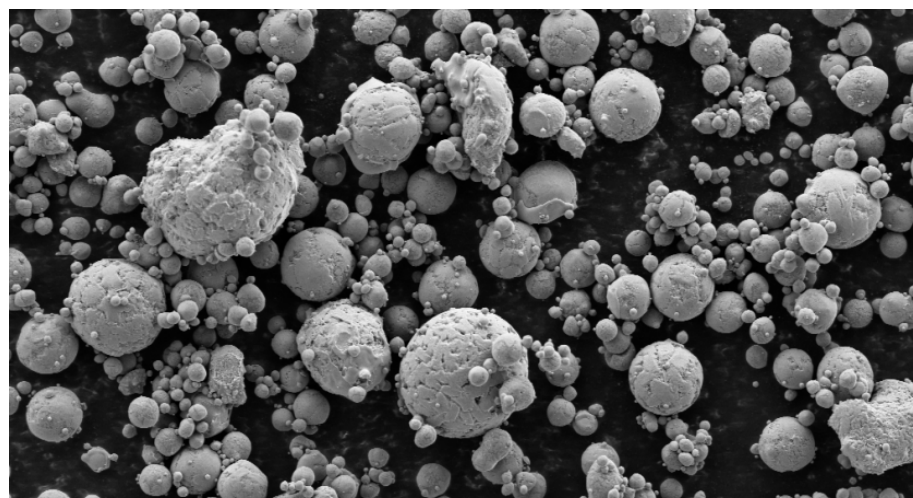


HER

NiAl (54:46 wt%) alloy  
NiAlMo (39:44:17 wt%) alloy

OER

NiAl (54:46 wt%) alloy  
NiAl +  $\text{Co}_3\text{O}_4$



10  $\mu\text{m}$

EHT = 5.00 kV  
NiAlMo, Lot 29269

WD = 8.4 mm

Mag = 500 X

Date : 8 Jul 2011  
Signal A = SE2

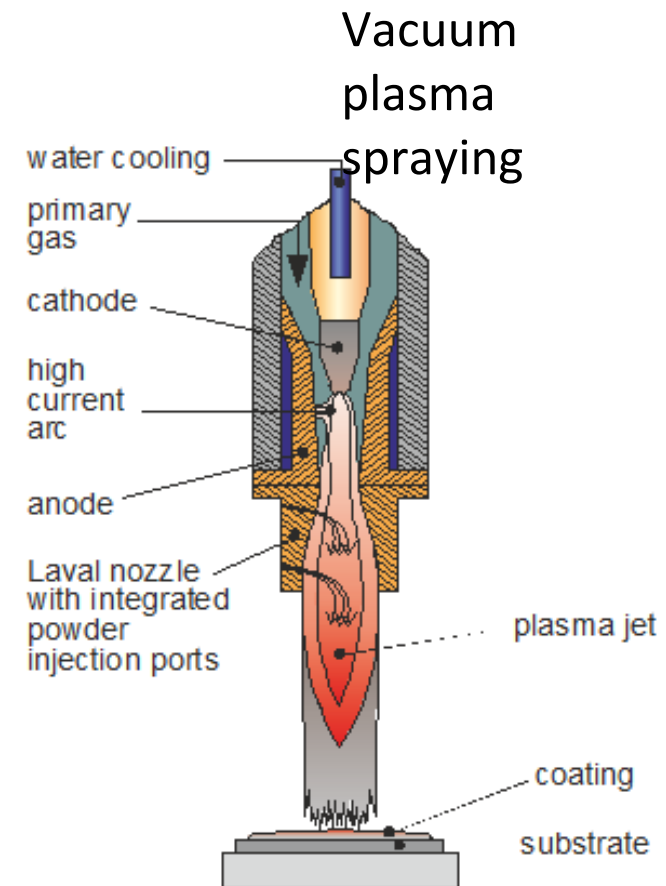
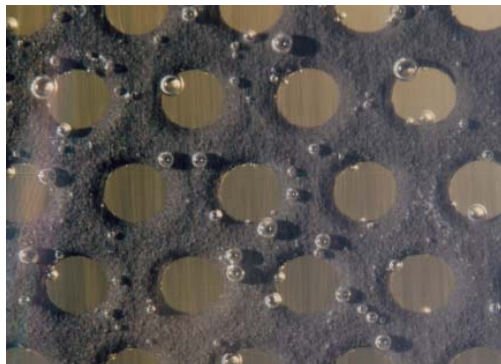




# VPS Raney Ni Coating

**Electrode development for low overpotential, long lifetime and low costs**

Using VPS coating technology electrodes were developed with low-cost materials that have a high efficiency/low overpotential and little degradation in intermittent operation

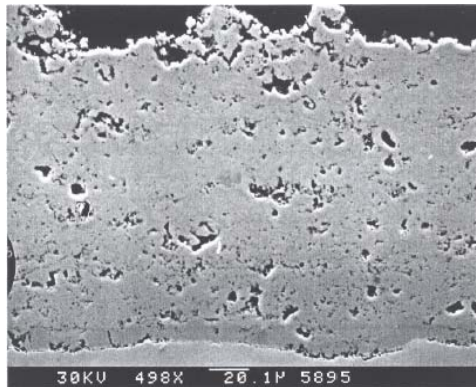


Deutsches Zentrum  
für Luft- und Raumfahrt e.V.  
in der Helmholtz-Gemeinschaft

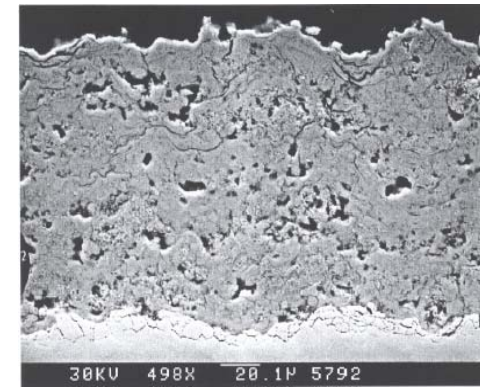


# VPS Raney Ni Coating

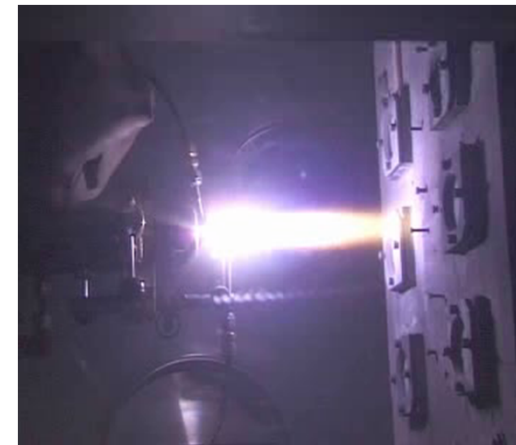
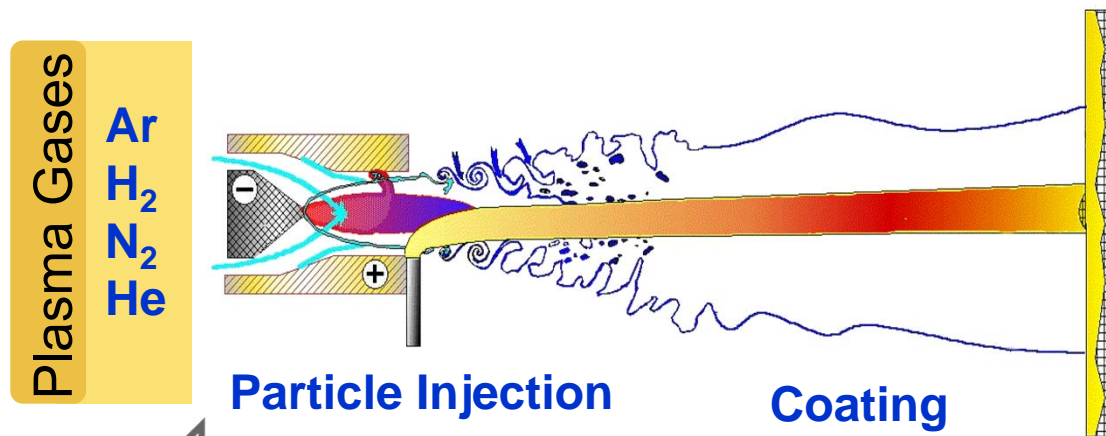
Plasma-sprayed Raney Nickel cathode before activation



Plasma-sprayed Raney Nickel cathode after activation



Principle of Vacuum Plasma Spraying



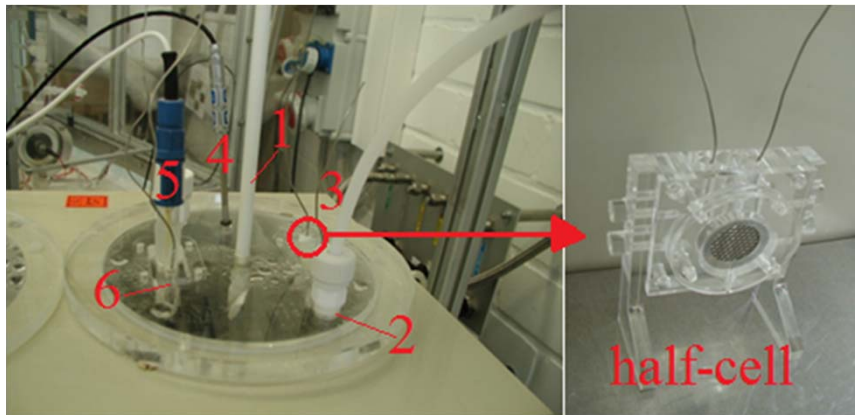


# Electrode Performance – Half Cell Test Configuration

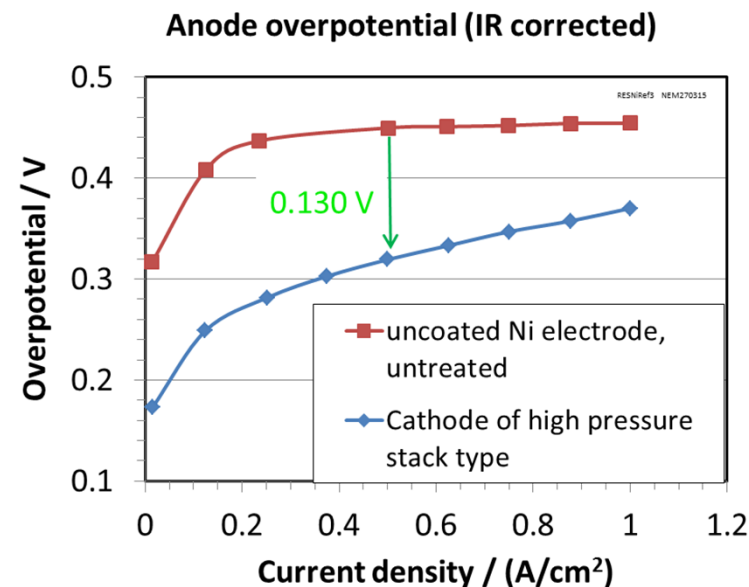
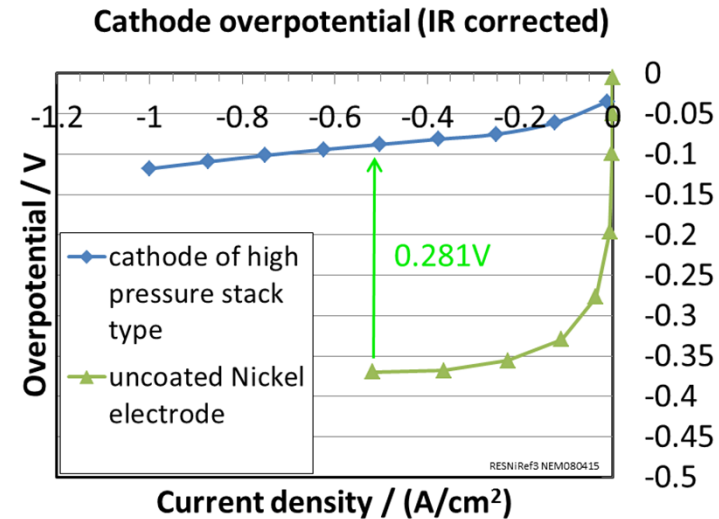
Half cell measurement

Electrode area: 4 cm<sup>2</sup> ; Cathode: NiAlMo

Anode: NiAl; Conditions: 70 °C, 30 wt.% KOH



1. Stirrer
2. Gas collector
3. Working electrode
4. Count-electrode
5. Reference electrode (Hg/HgO)
6. Thermocouple



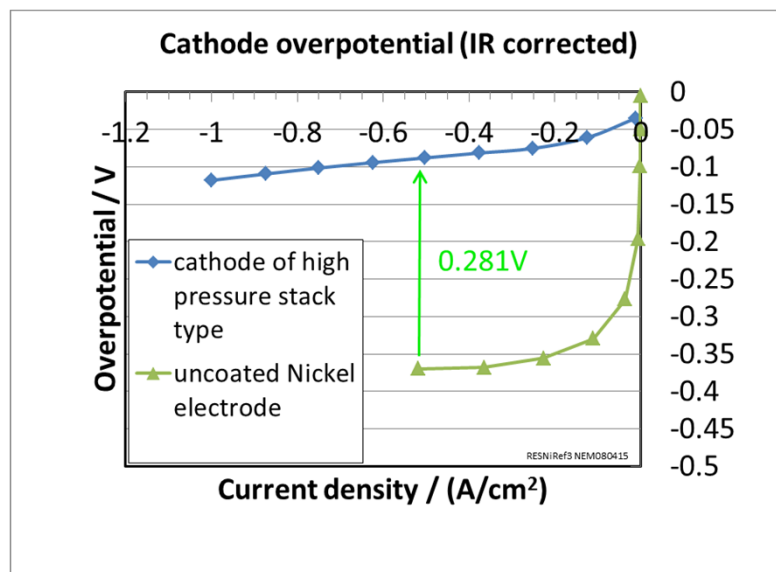
# Electrode Development for Low Overpotential, Long Lifetime and Low Costs

## Progress achieved:

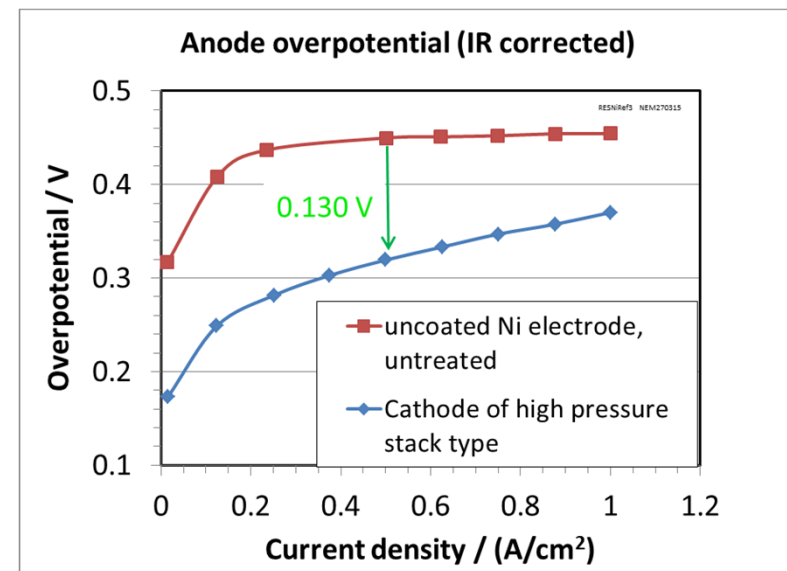
Long term test in intermittent operation,  $0.5 \text{ A/cm}^2$ ,  $70^\circ\text{C}$ :

- After 1100 on-off cycles

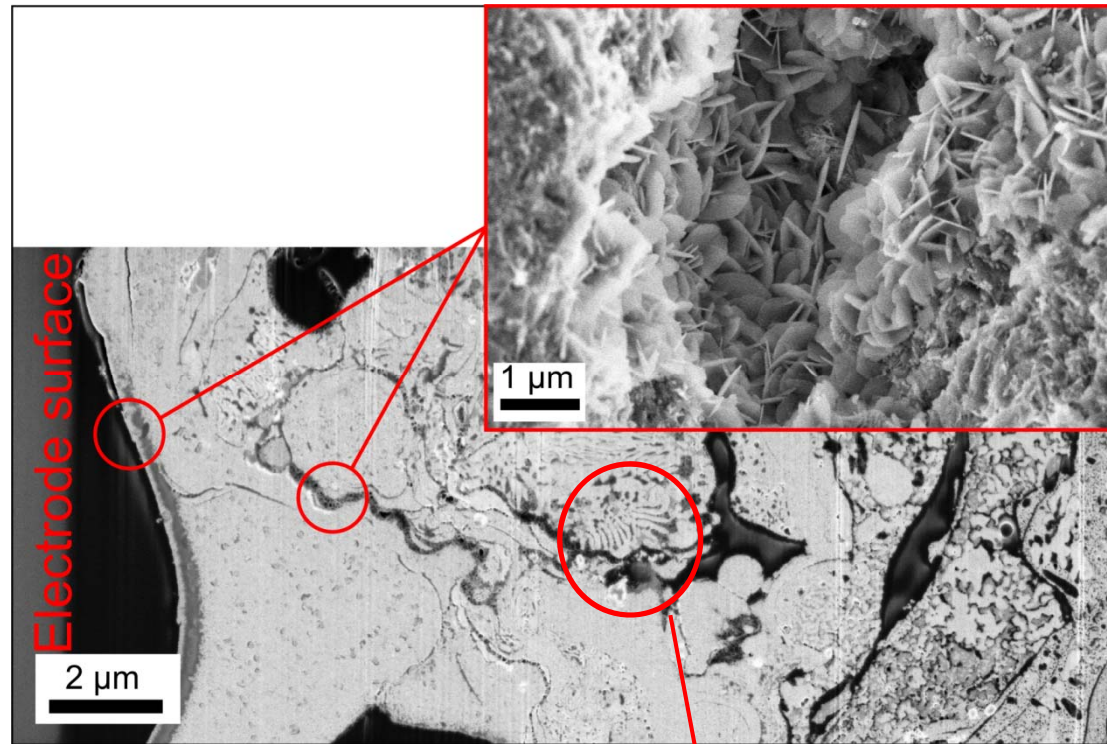
cathode -10 mV



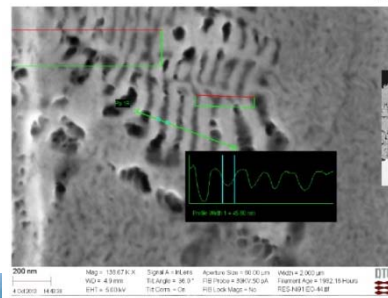
anode + 23 mV,



# Investigation of Electrode Microstructure

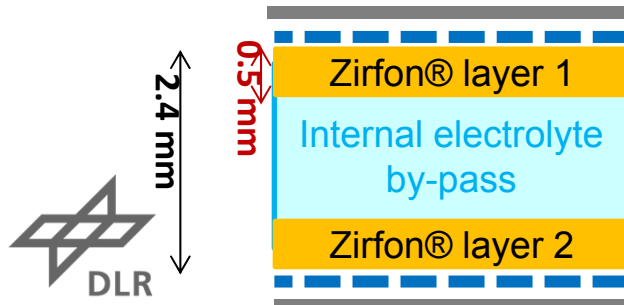
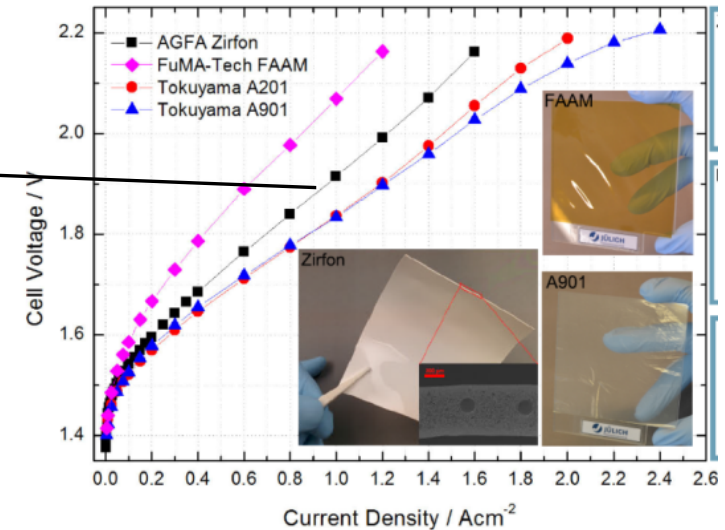
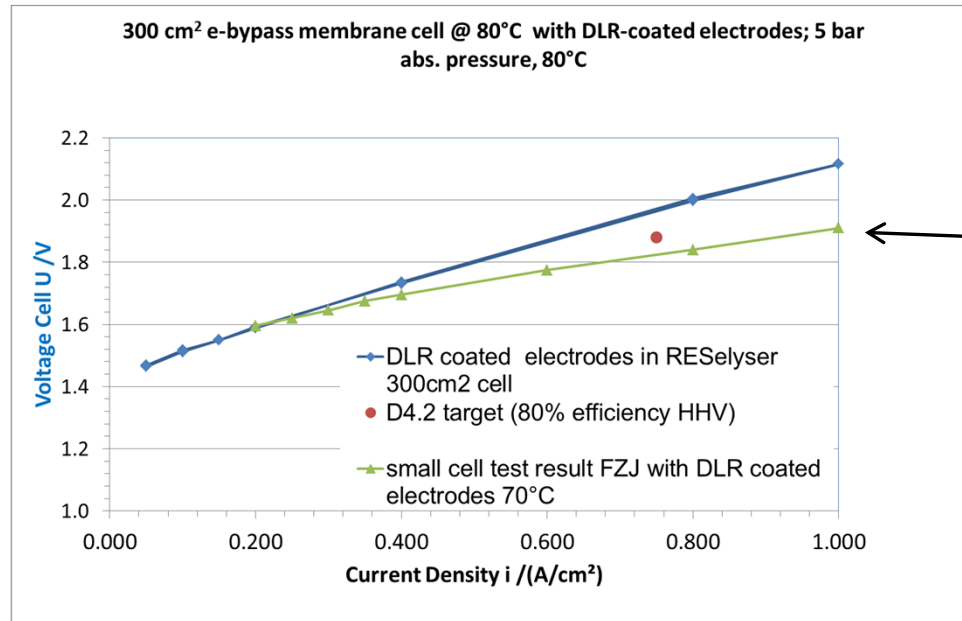


- Highly heterogeneous microstructure with many subdomains.
- Dendritic structures stemming from the dissolution of Al from the Raney type NiAl alloy particles.
- Desert rose like nano flake structures ( $\text{Ni}(\text{OH})_2$ ) observed in the pores especially after long term operation





# Electrode Performance – Full Cell Test



- Double side coated PPS spacer-fabric, Zirfon® (ZrO<sub>2</sub>/polymer composite) dual layer
- Variation of permeability of Zirfon layers: from 120 l/(h m<sup>2</sup> bar) to 900 l/(h m<sup>2</sup> bar)
- Separators of 300 cm<sup>2</sup> delivered for cell and stack integration
- Technical scale (2500 cm<sup>2</sup>) producibility demonstrated





# Electrode Fabrication by Air Plasma Spraying

- Variation of coating parameters by using an industrial-type APS torch (Triplex)
  - > significant cost reduction compared to VPS
- Impact on coating porosity by varying gas flow rates and hence particle velocities

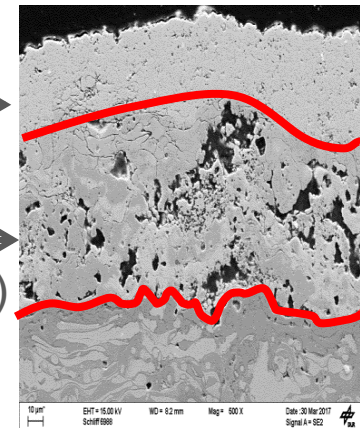


Standard APS Torch

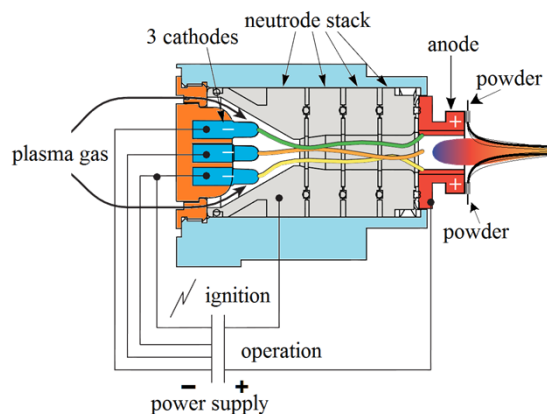
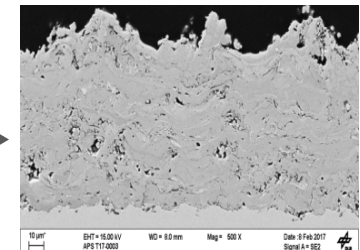


Flame: 30 mm - 100 mm  
T: 2000 °C; v: < 300 m/s

VPS →



APS  
(standard) →

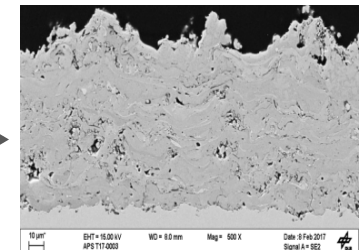


APS Triplex Torch



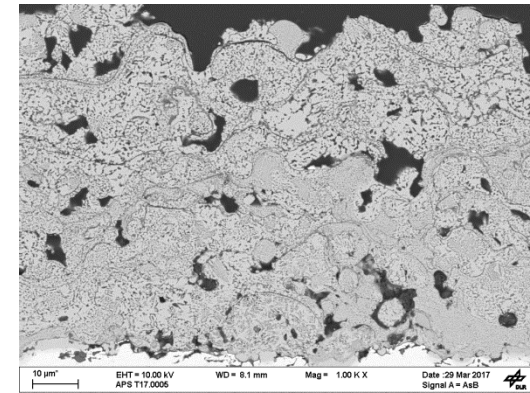
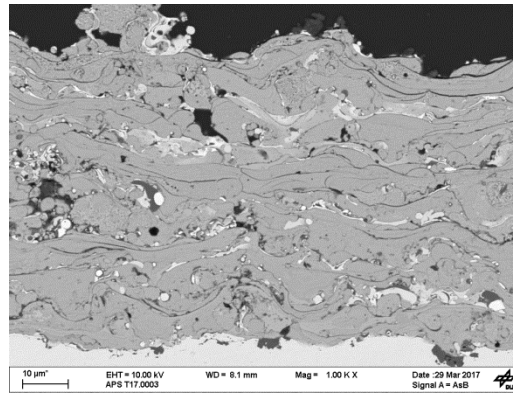
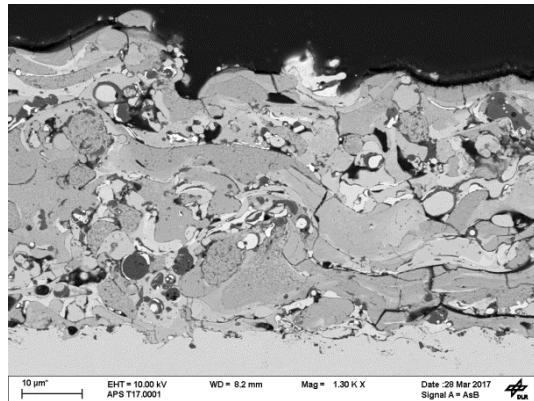
Flame: 50 mm – 200 mm  
T: 3000°C; v: < 700 m/s

APS  
(Triplex) →



# APS Electrodes Performance – Half Cell Configuration

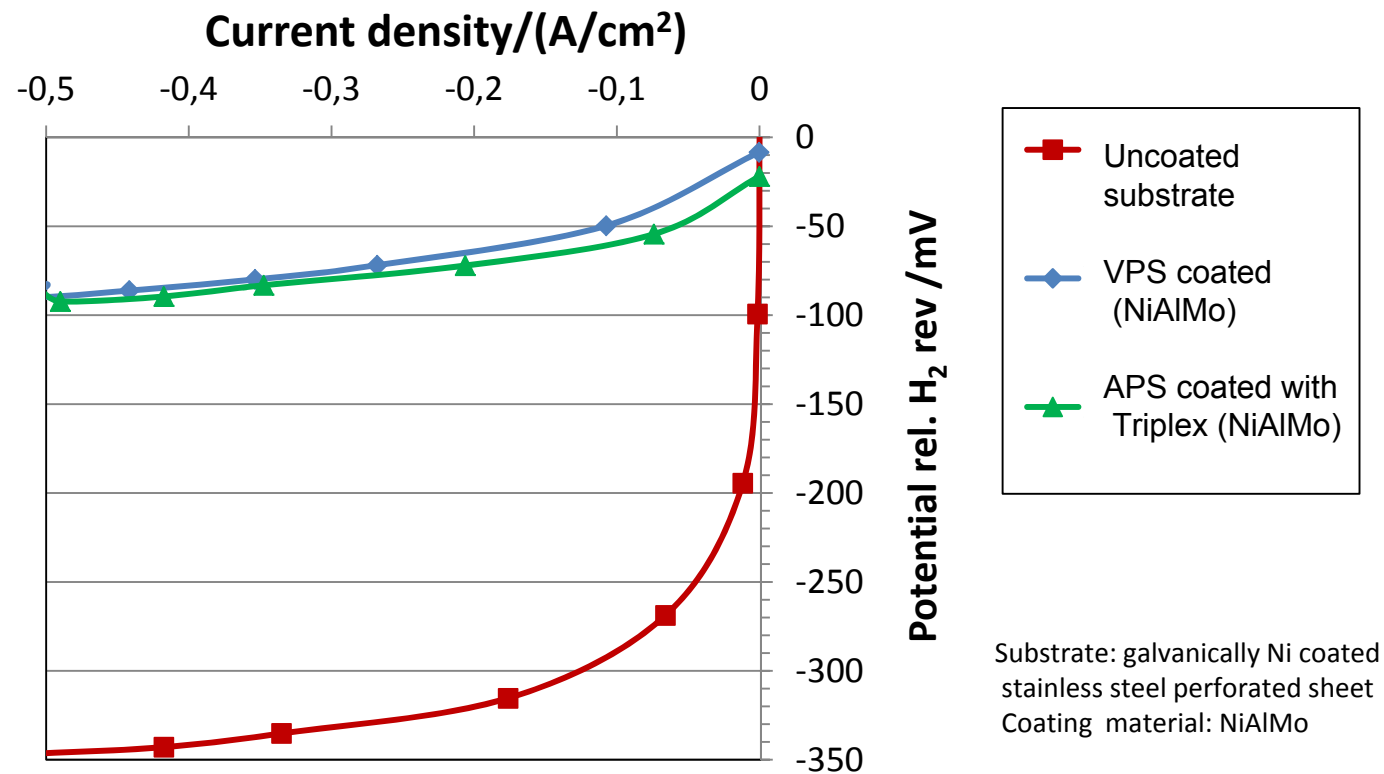
NiAlMo coating cross section after spraying with APS Triplex with different particle velocity and activation



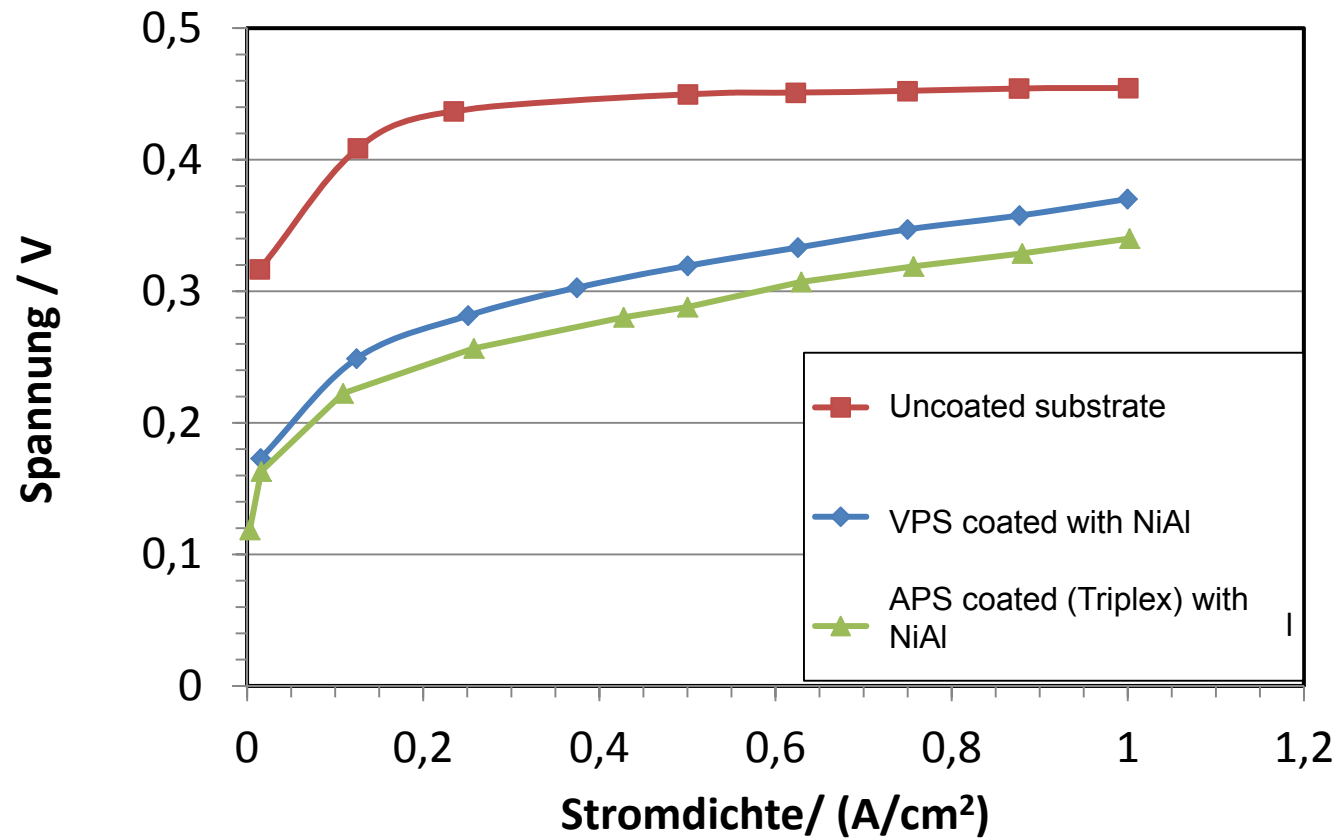
Plasma in-flight particle velocity →



# Recent Electrochemical Results of Coated Cathodes



# Recent Electrochemical Results of Coated Anodes





# Power-to-Gas Plant in Wyhlen, Germany

## Planning of Site



Source: Energiedienst

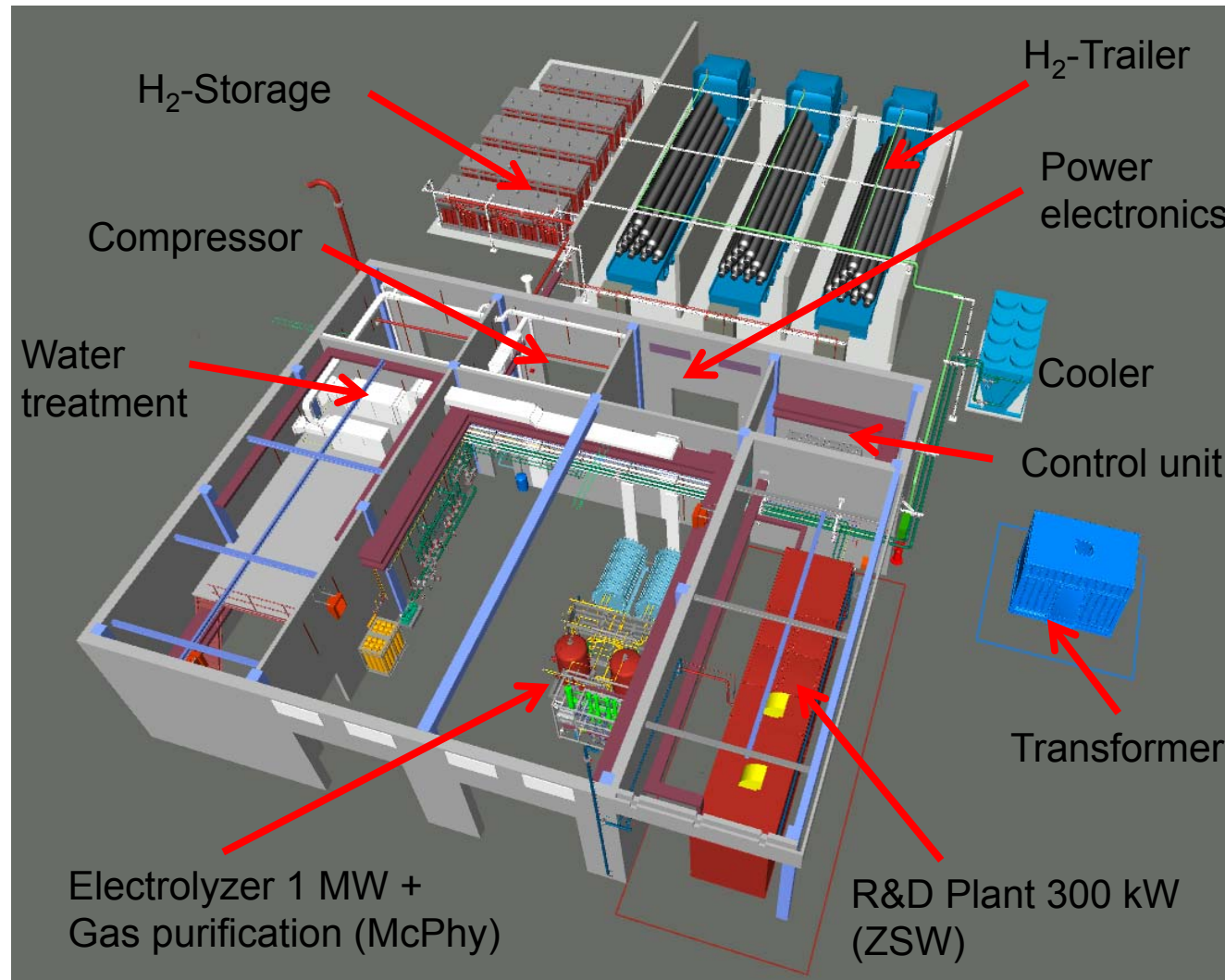






# Power-to-Gas Plant in Wyhlen, Germany

## Planning of Site



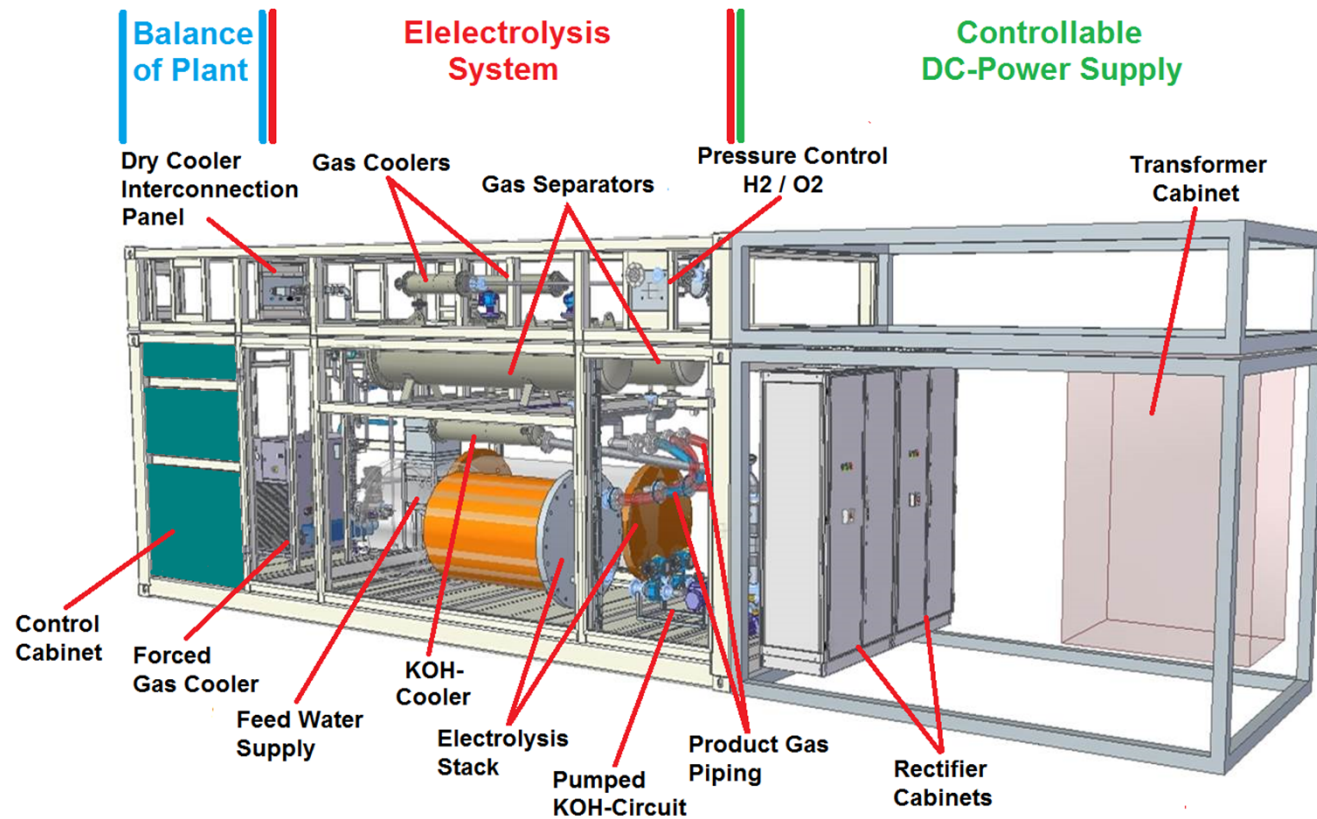
Source: Energiedienst / Haas Engineering





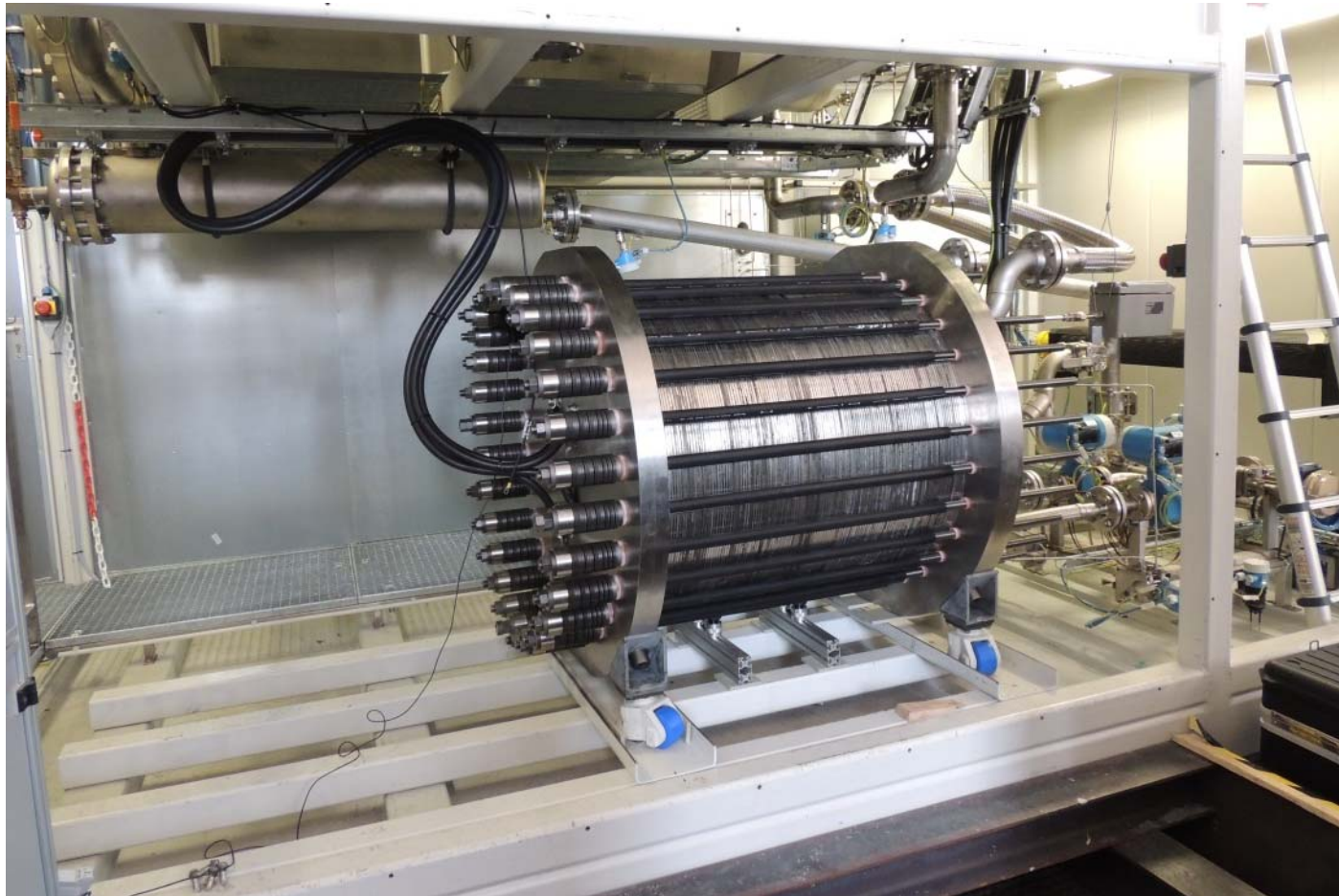
# Light House Project „Power to Gas“

## Pressurized Alkaline Electrolyzer of ZSW





## Advanced Alkaline Electrolysis Stack of ZSW (300 kW Stack for Pressurized Operation)



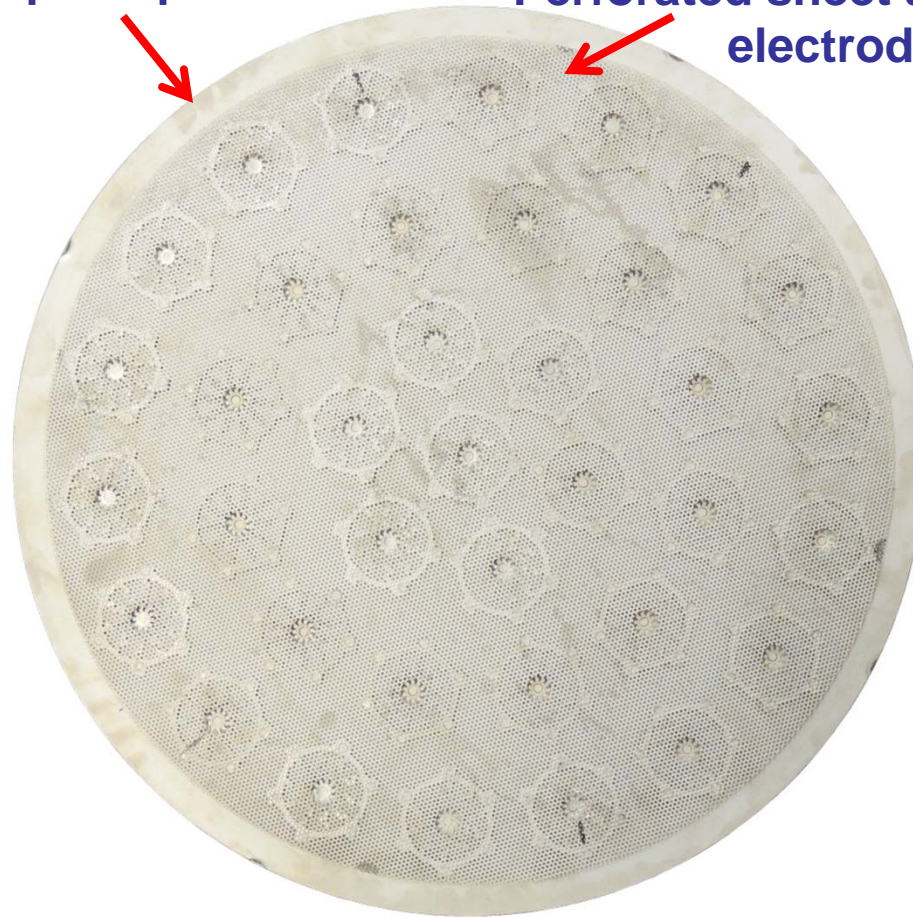




## 3000 cm<sup>2</sup> Electrode Packages (Effective area 2750 cm<sup>2</sup>) for Pressurized Alkaline Electrolyzers

Bipolar plate

Perforated sheet as working  
electrode



# Summary

- Based on former experience DLR continues with the development of efficient and cost-effective electrodes for alkaline water electrolysis.
- Hydrogen and oxygen evolution electrodes using Raney alloy materials are developed by applying plasma spray technology and are electrochemically characterized.
- Low cell voltage around 1.8 V at a current density of 0.6 A/cm<sup>2</sup> was achieved.
- The change from vacuum plasma spraying to atmospheric plasma spraying results in a significant cost reduction for electrode fabrication.
- Electrodes with a size of 3.000 cm<sup>2</sup> will be manufactured in the coming months to equip a 300 kW electrolyzer for a power-to-gas R&D plant in the frame of the lighthouse project „P2G-BW“



# Acknowledgment

Financial support through the Ministry of Economics of the State of Baden-Württemberg (Lighthouse Project „Power-to-Gas-BW“) and the FCH-JU Project „RESelyzer“ (Contract N° 278732) is gratefully acknowledged.



Special thanks also to:

**Andreas Brinner**



**Jake Bowen**



**Marcelo Carmo**



# Thank you



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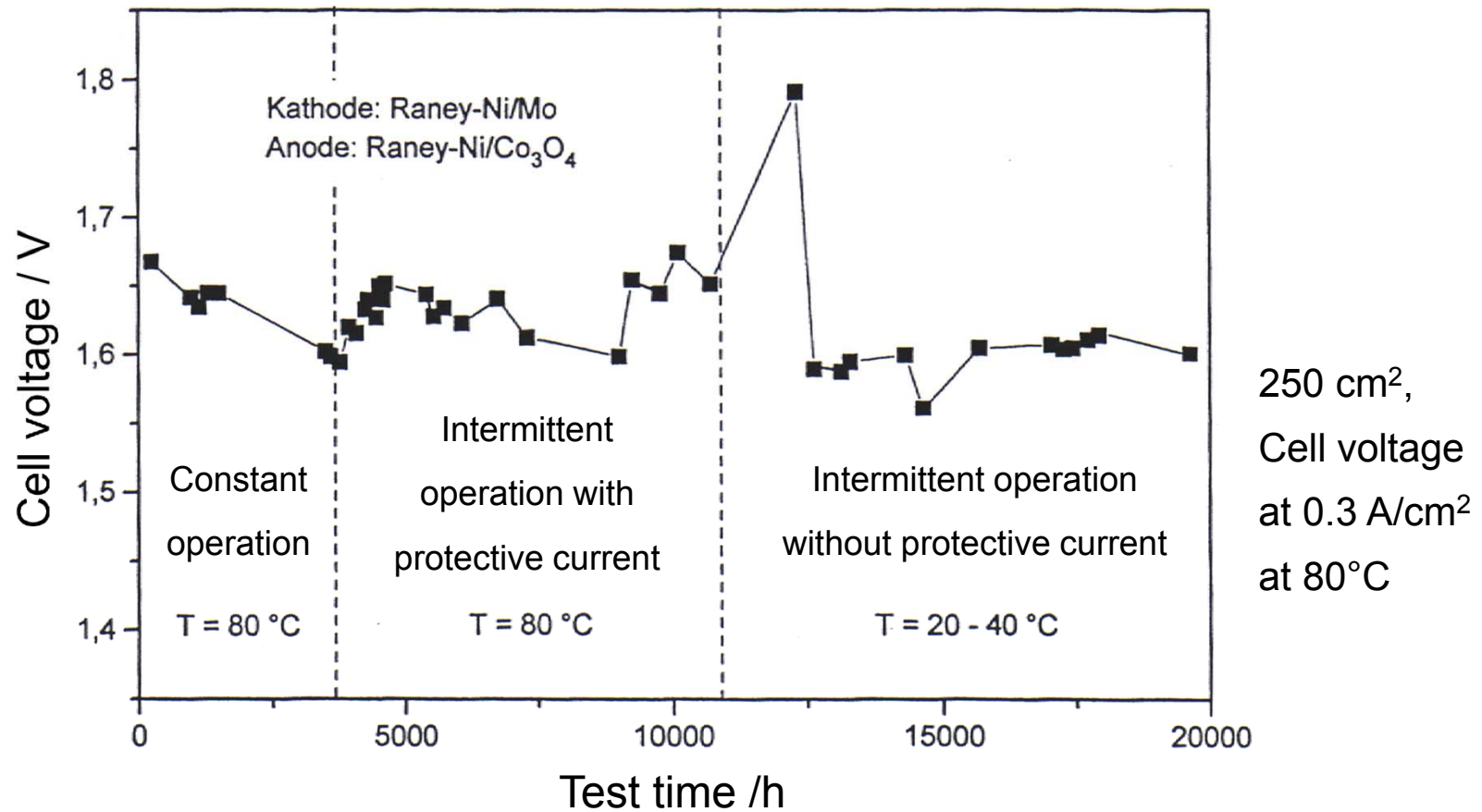


## APS vs VPS Electrodes Cost

	VPS	APS
Yield per day	3 m <sup>2</sup>	3 m <sup>2</sup>
CAPEX	2,8 million €	0,480 million €
Depreciation time	10 years	10 years
Machine cost per day	1272 €	218 €
Other operating costs per day	212 €	196 €
Machine + other operating cost per m <sup>2</sup>	494 €	138 €
Staff cost per day	528 €	528 €
<b>Coating cost per m<sup>2</sup></b>	<b>670 €</b>	<b>314 €</b>

**Cost reduction from VPS to APS can be above 50% and as much as 72%**

# Long-Term Tests of Single Cell VPS Coated Electrodes at DLR



# Long-Term Measurement with Plasma Sprayed Electrodes

Time evolution of cell voltage with plasma-sprayed electrodes ( $600 \text{ cm}^2$ ) at reference conditions ( $300 \text{ mA/cm}^2$ ,  $80^\circ \text{ C}$ )

